Proceedings of the 4th International Conference of Fluid Flow, Heat and Mass Transfer (FFHMT'17)
Toronto, Canada – August 21 – 23, 2017
Paper No. 183
DOI: 10.11159/ffhmt17.183

Discharge Coefficient Behaviour in Presence of Four Perforated Plates Flow Conditioners

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Abstract **-** This paper present a numerical experimentation of the behaviour of the discharge coefficient and the effect of four perforated plates like flow conditioners on the discharge coefficient for flow measurement accuracy. Three of the plates are described by the Standard ISO5167 and the fourth one is proposed for study. The flow is subject to two disturbers namely 50% closed valve and 90° double bend in perpendicular planes. The turbulent flow is examined in conduit with an inner diameter of D=100mm. The diameter of orifice meters are respectively d=50, 60, 70 and 75mm which done for β ratio d/D respectively the values of 0.5, 0.6, 0.7 and 0.75. The orifice meters are located in conduit at different stations z/D downstream the disturbers. The flow is examined with air at Reynolds number $Re=2.5x10^5$. The results showed that the perforated plates have significantly reduced the error on the discharge coefficient. Indeed, the errors recorded downstream disturbers are superior to 12%. Downstream the perforated plates used separately the errors on the discharge coefficient are reduced to a value inferior to 1% for the four plates. It is noted that the standards ISO5167 and AGA3 stipulate that the error on the discharge coefficient Cd must be less than 0.5% for better flow measurement accuracy. By comparing our results with this condition we found that the error obtained on the discharge coefficient with the four perforated plates are substantially reduced especially downstream station z=25D (z =19D downstream disturbers). However the fourth proposed plate with its height porosity produces less lose pressure than those of the other three plates. This is good conditions of exploitation for some installation where height lose pressure are not tolerated.

Keywords**:** Perforated plates flow conditioners, flowmetring, discharge coefficient.

1. Introduction

The majority of the orifice meters must be calibrated. This is done in fully developed pipe flow, axisymmetric pipe that is free from swirl and pulsation. Standards such as ISO5167 [1] define a satisfactory flow. While high accuracy about 0.5% flow rate measurement is required, disturbances in the flow caused by valves, bends, and other component introduce errors of more than 3%.

Given that most industrial installations include disturbers like bends, valves, expanders and reducers, which are sources of swirl, asymmetries and turbulence distortions, insuring that fully developed flow in terms of mean flow and turbulence structure approach the meter is difficult to achieve in practical situations.

For best accuracy, a flow meter needs to be presented with an axisymmetric, fully developed velocity profile with zero swirls. Either very long lengths of straight pipe work upstream of the flow meter must be provided as recommended by standards ISO 5167 and AGA-3 [2], these may need to be of the order of 80 to 100 pipe diameters, which will give a higher installation cost and greater space requirement.

Research work by Gallagher J. [2], T.T. Yeh and G. Mattingly [3], Laribi B. and al [4-7], R. Rans [8], Darin L. and Bowles E. B. [9], F. Sharipov [10] and more recently Laribi B. and al [11] have reported a number of computational studies of installation effects on orifice meter performances.

Our paper examines the effect of for perforated plates with orifice meters on the shift deviation of the discharge coefficient for best metrological performances basing on the pressure drop across the orifice in non-standard conditions.

The investigation is conducted to show the effect of the two disturbers namely a 90° double bends in perpendicular planes and a 50% closed valve on the deviation of the discharge coefficient.

2. Turbulence Models

The general equation used in CFD code is given by Eq. 1 as bellow:

$$\frac{\partial}{\partial t}(\rho\phi)+\nabla U\phi=\nabla\left(\Gamma_{\phi}grad\phi\right)+S_{\phi} \qquad (1)$$

Where:

ϕ a general variable which can be velocity U ($m.s^{-1}$), turbulence kinetic energy k ($kg.m^{-2}.s^{-2}$) or the dissipation rate ε($m^{-2}.s^{-3}$).

ρ is the density of fluid ($kg.m^{-3}$).

Γ_ϕ is the diffusion coefficient of the variable ϕ.

S_ϕ is the source term of the variable ϕ.

The turbulence model used for this simulation is k-ε model. It is the simplest and complete model known as two equations. This model assumes that the turbulent regime is fully established throughout the area and that the effects of molecular viscosity are negligible compared to the turbulent viscosity (away from walls). It is based on the Boussinesq hypothesis. It is a semi-empirical model. Two transport equations are used, one for the turbulence kinetic energy k and the other for its dissipation rate ε. The reader can consult the literature Fluent [12] for thorough study.

3. Experimental Facility for the Simulation

3.1. Air Flow Rig

The basic experimental facility is presented in figure 1. It consists of a long conduit pipe with 100 mm inner diameter. The air enters the pipe then flows through a straight pipe of 10D length, which is followed by disturbers. The 90° double bend in perpendicular planes and 50% closed valve were used separately. The orifice meter diameters used in this simulation are respectively d= 50, 60, 70 and 75mm diameters which done for β ratio d/D respectively the values of 0.5, 0.6, 0.7 and 0.75. The first orifice meter is installed at 97D downstream of the flow disturber, where the flow is fully developed. Stations used for the second orifice meters are respectively 1.5D, 7D, 12D, 17.5D, 25D, 35D downstream the disturber.

The two orifice meters have standard geometry. A length of 10D is provided downstream the entrance of flow and downstream the orifice meter installed at station 91D for natural flow development. The Reynolds number of the turbulent flow is 2.5×10^5.

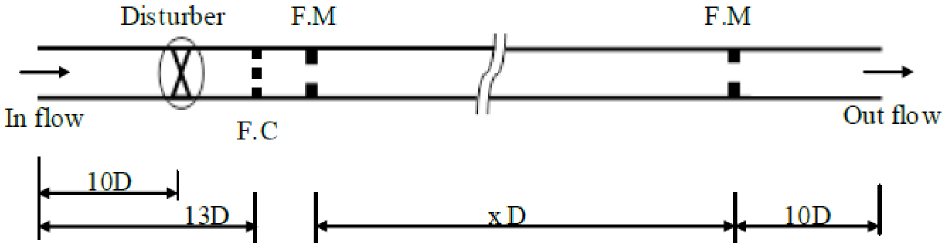
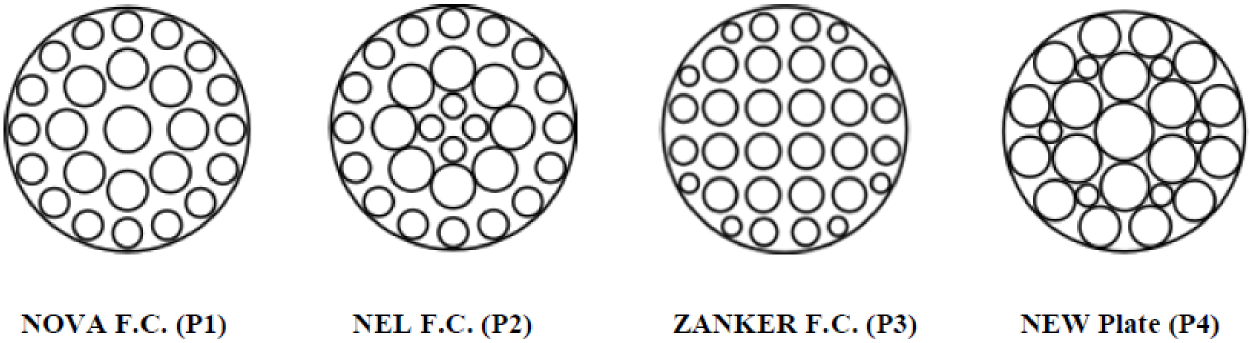


Fig. 1: Conduit.

3.2. Perforated Plates used in simulation

The three perforated plates flow conditioners (F.C.) used in the study and described by the Standard ISO5167 are shown in figure 2. The forth one is our proposed plate.



NOVA F.C. (P1)
NEL F.C. (P2)
ZANKER F.C. (P3)
NEW Plate (P4)

Fig. 2: The four perforated plates.

3.3. Variation of the Discharge Coefficient

For testing the effect of disturbers on the discharge coefficients of the orifice meters, the shift deviation for the discharge coefficient ΔCd (%) is calculated by using the difference pressure □P obtained by the simulation at different locations of the orifice meter in the pipe and □Po at the same time at station z/D=97 were the flow is fully developed. Eq. 2 shows the calculus formula:

$$\Delta Cd(\%) = \sqrt{\frac{\Delta Po}{\Delta P}} - 1 \tag{2}$$

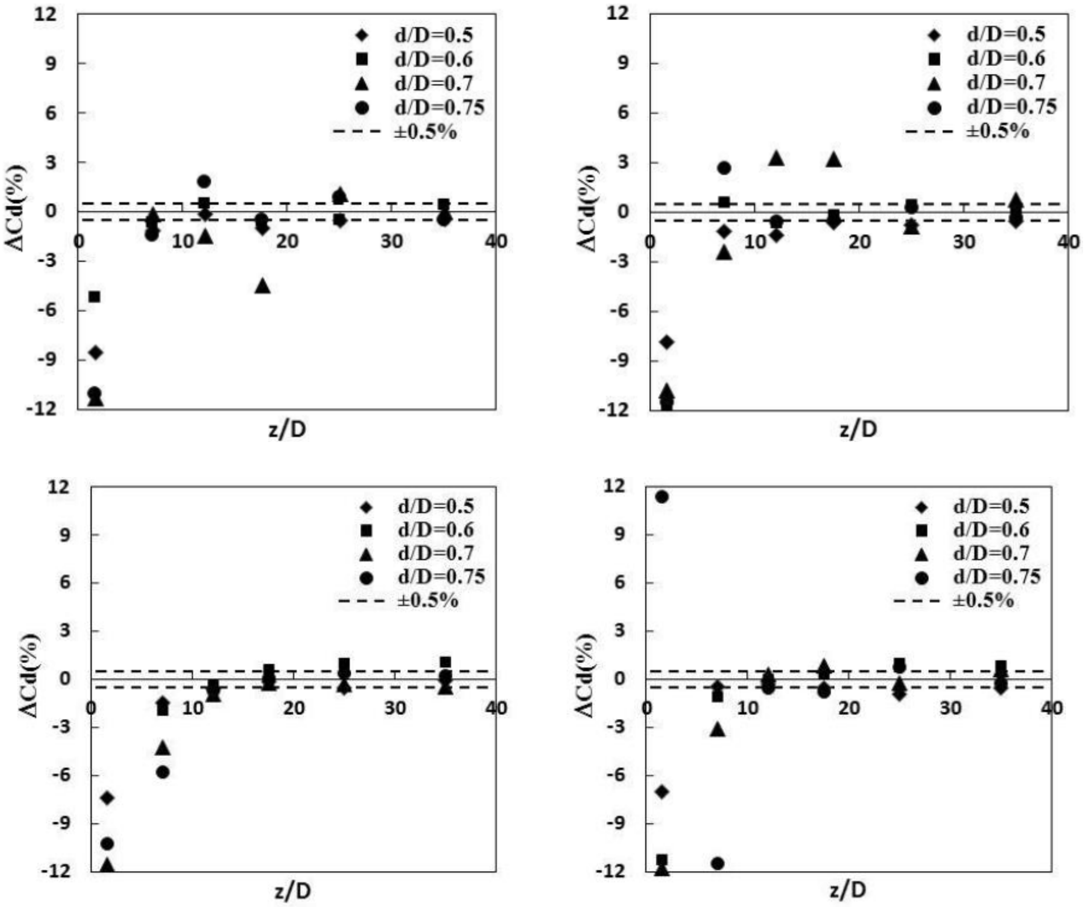
The difference pressure is calculated according to the standard ISO 5167 at D upstream and D/2 downstream the orifice meter. This formula was applied for the four orifice plates with the two disturbers.

4. Results and Discussion

4.1. Discharge Coefficient Errors with 50% Closed Valve on Line and Perforated Plates

Experiments were conducted to determine the relative change in the orifice meter discharge coefficient when subjected to non-standard approaching flow conditions like 50% closed valve. The test sections were 1.5D, 7D, 12D, 17.5D, 25D, 35D downstream the valve. The effect of valve on the orifice meter with the four orifice meters with β= 0.50, 0.60, 0.70 and 0.75 respectively at Reynolds number of 2.5×10^5 is shown in figure 3. The principal remark shown in this figure is that at station z/D=1.5 when β increases, ΔCd (%) increases. This situation is the same in presence of the four perforated plates used in this numerical study.

Indeed, we register at station z/D=7 a value close to zero for ΔCd (%) with β=0.5 with the NOVA F.C. This value increases to reach a mean value more than 3% for β=0.75 with the other flow conditioners. We have to remember that the Standard ISO 5167 recommend a maximum value for ΔCd (%) of 0.5%. Our results are in good agreement with the standard for station z/D=17.5 and more for the four flow conditioners. This result let's suppose that if we would like to get a good flow measurement, the orifice meter must be placed at station z/D=25 or more downstream the valve.

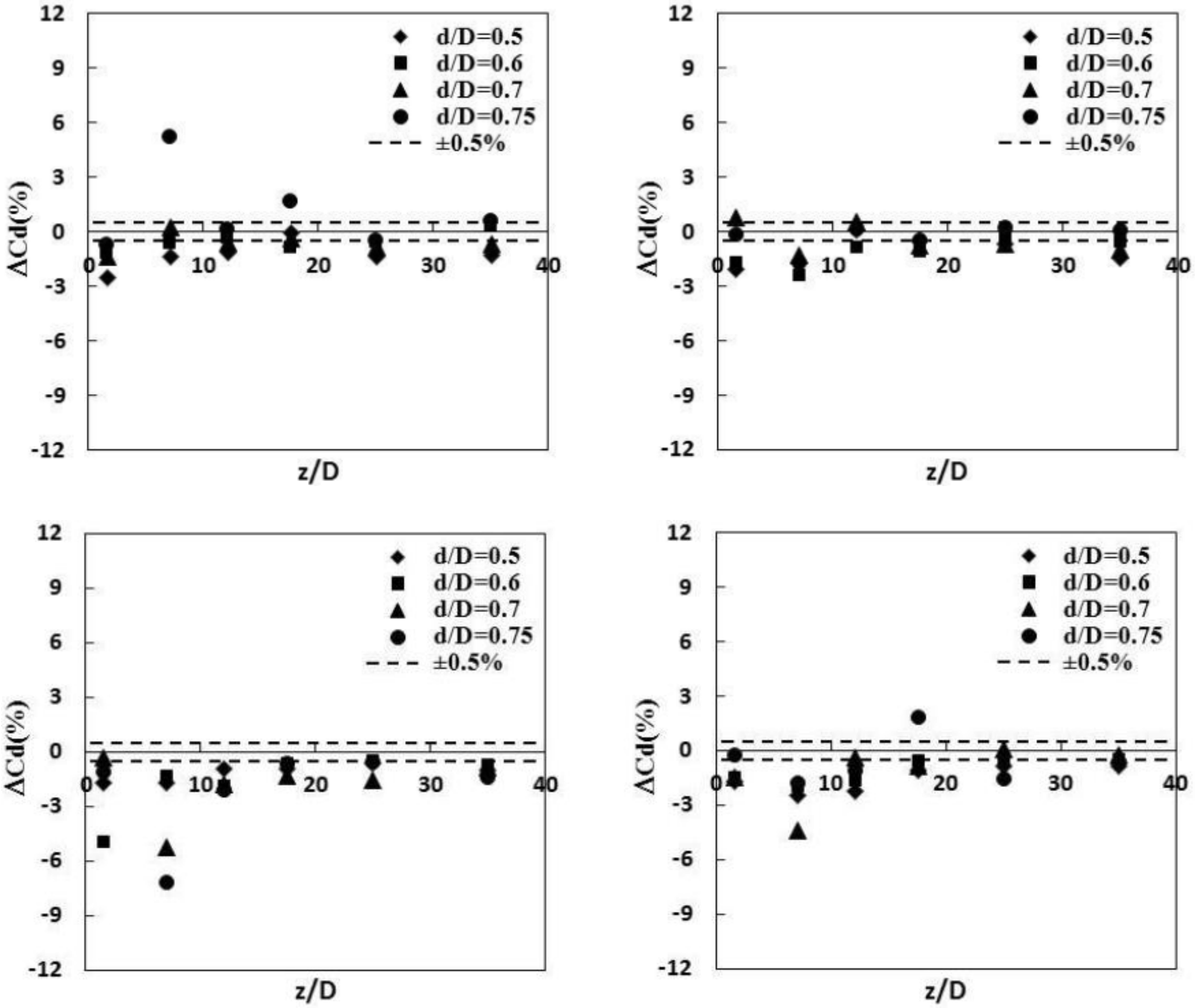


ZANKER F.C. (P3) **NEW Plate (P4)**

Fig. 3: Discharge coefficient errors for the four F. C. with valve 50% closed.

4.2. Discharge Coefficient Errors with Double Bend on Line

In this case, experiments were conducted to determine the relative change in the orifice meter discharge coefficient when subjected to 90° double bend in perpendicular planes. The test sections were 1.5D, 7D, 12D, 17.5D, 25D, 35D downstream the double bend. The effect of this disturbers on the orifice meter with the four orifice meters with β= 0.50, 0.60, 0.70 and 0.75 respectively with a Reynolds number of $2.5x10^5$ is shown in figure 4. The principal remark shown in this figure is the same which obtained with the valve. Indeed, when β increases, ΔCd (%) increases especially at station z/D=7. This situation is the same for the four perforated plates used in this study. We register at station z/D=7 a value close to 0.3% for ΔCd (%) with β=0.5 with NOVA F.C. and reach a mean value 2.7% for β=0.75 for the NEL F.C. Our results are in good agreement with the standard for station z/D=25 and more. This result is the same of results obtained for the valve.



ZANKER F.C. (P3)

NEW Plate (P4)

Fig. 4: Discharge coefficient errors with double bend 90_o on line.

5. Conclusion

The present numerical investigation examines the effect of upstream conditions on orifice meters otherwise on the discharge coefficient Cd. The flow is disturbed by a 50% closed valve and a 90° double bend in perpendicular planes used separately. The discharge coefficient were measured with four different orifice meters with β=0.5, 0.6, 0.70 and 0.75 at Reynolds number Re=$2.5\text{x}10^5$.

The principal result shows that when β increases the shift deviation on the discharge coefficient ΔCd (%) increases. This result is the same with the two disturbers. Indeed if we would like to get a good flow measurement, the flow meter must be located at distance z/D=25 downstream the disturber or more. In this situation, a good agreement is obtained with the standards ISO 5167.

We also concluded that the valve 50% closed could be considered for further experimental investigations than the 90° double bend in perpendicular planes which gave minimum errors (minimum disturbances) on the discharge coefficient contrary to the valve.

At last, the CFD shows their efficiency to predict the flow behaviour in different situations and let us to plain our experimental study in optimal conditions in order to validate the numerical investigations.

Acknowledgements

This study is a part of a research project approved by the Algerian Ministry of Higher Education and Scientific Research under number J0303920130026. The authors acknowledge the High Ministry of Education and Scientific Research of Algeria for supporting financially this project.

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