The Fluid Dynamics of Rising and Evaporating Droplet in an Immiscible Liquid

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Abstract - Analytical solutions were obtained for the virtual mass coefficient, drag coefficient and the equation of motion of an evaporating drop and a growing bubble within the drop that rises in an immiscible liquid. The derived theoretical results were agreeable with the available experimental data.

Keywords: Direct-contact heat transfer, Bubbles, Evaporating drop, Virtual mass coefficient, Drag coefficient.

1. Introduction

Direct-contact heat transfer between a drop rising and vaporizing in a continuous, stagnant and immiscible liquid whose temperature is above the boiling point of the drop has extensive applicability in a number of engineering fields. One of the important applications is the process of desalination of sea or brackish water by freezing. The phenomenon is complicated due to continuous evaporation of an immiscible hydrocarbon droplet during its rise. This makes its size changing with time as shown in Fig.1. Since the velocity of rise of bubble or drop is a strong function of size and the size is expanding, hence the velocity becomes a function of time.
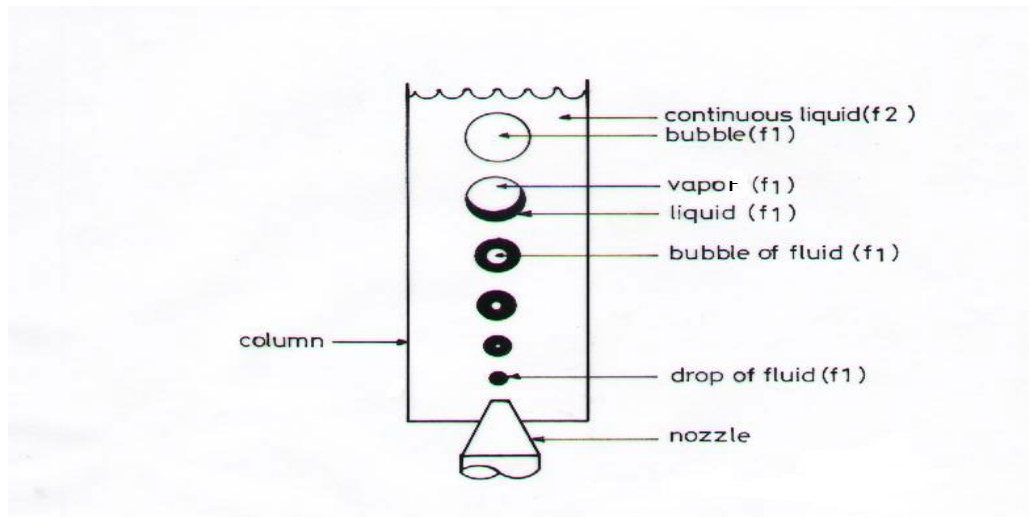

Fig. 1 Schematic sketch of an evaporating drop in an immiscible liquid

Simpson et al. [1] showed experimentally that the instantaneous velocity of the evaporating butane droplet was constant at about 0.25m/s up to a diameter ratio of 2.0 in brine and 2.7 in water. Thereafter, the velocity varied as the square root of the diameter ratio. This ratio is between the instantaneous diameter and the inlet drop diameter. Selecki and Gradon [2] transformed the equation of motion into a Ricatti type and solved it numerically to obtain the travel distance of

the drop as a function of time. They used ½ as the value of the virtual mass coefficient in their solution which was agreeable with their experimental data. The only analytical solution, as far as another is aware, is that of Raina and Wanchoo [3] who derived an equation for the velocity of rise of the drop, simply, by equating the drag to buoyancy. This equation is not easy to use due to its complex type. The following facts were not taken into account during the derivation:

(i) The buoyancy due to the vapor within the drop.
(ii) The virtual mass of the two-phase drop.
(iii) The transient motion of the drop.

The pioneer works of Shimaoka and Mori [4] produced a correlation for the instantaneous velocity of the liquid/vapor two-phase bubble. The finite element method in Langrangian from was applied by Dammel and Beer [5] to solve the Navier-Stokes equations. They found a vortex generated within the liquid of the drop as it rises up inside the immiscible liquid

The aim of the present work is to get more understanding of the hydrodynamics associated with the evaporation droplet during its rise with heat absorption from the continuous phase. This will be achieved through the analytical solution of the equation of motion by considering the virtual mass effect, that was not considered earlier, and the interfacial drag forces.

2. Theoretical analysis
2.1 The virtual mass of the evaporating droplet

Consider the system of the drop of diameter 2b and density ρ_{f1} (as shown in Fig. 2) and its nucleating bubble of diameter 2a and density ρ_{g1}. Assume that the two spheres are concentric. This configuration was classified by Mori [6] and Oguz and Sadhal [7] as one of the possible configurations encountered in direct-contact evaporation of volatile drops in an immiscible liquid.

The irrotational and inviscid flow of the two concentric spheres were given by Lamb [8] and utilized by Kendoush [9]. The total kinetic energy of the fluid surrounding the drop is given by the following (Lamb [8])

$$KE = \frac{1}{3}\pi\rho_{f1}\frac{U^2 a^3(1+2x)}{(1-x)} \qquad (1)$$

where

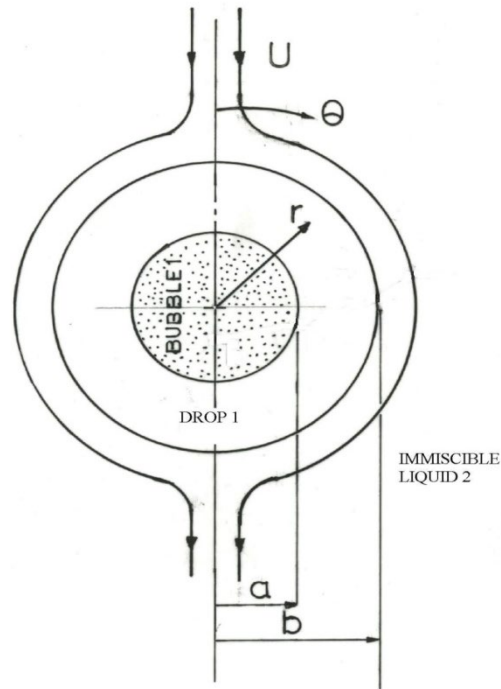$$x = (\frac{a}{b})^3 \qquad (2)$$

Fig. 2 The geometry of the problem

where a is the radius of bubble1 in Fig. 2. Note that the parameter x can be interpreted as the vaporization ratio as given in Appendix A. If we put the kinetic energy as $KE = \frac{1}{2}MU^2$, then the virtual mass of drop that contains a small bubble inside it, becomes the following by using Eq. (1)

$$M = \frac{2}{3}\pi\rho_{f2}\frac{a^3(1+2x)}{(1-x)} \tag{3}$$

The virtual mass coefficient is defined according to Cheng, Drew and Lahey [10] by the following

Cv = volume of "virtual mass" ÷ volume of fluid displaced by the evaporating drop

By using Eq. (3), we get the following

$$C_v = \frac{(1+2x)}{2(1-x)} \tag{4}$$

This is a new equation that has not been reported before. As x→ 0 , we recover the value of $C_v = 0.5$ which is the virtual mass coefficient of the single sphere as given by Lamb [8]. This equation is illustrated in Fig. 3.
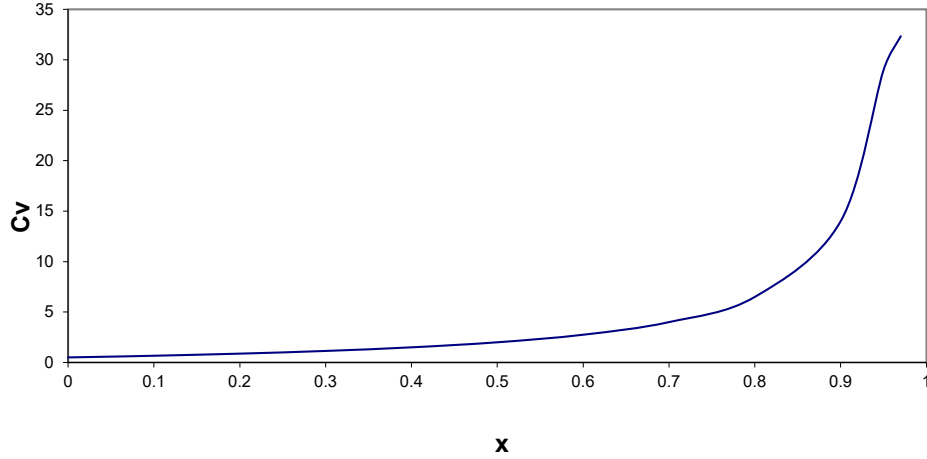
Fig.3 The relationship between the virtual mass coefficient and the vaporization ratio
according to Eq.(4).

2.2 The drag force on the evaporation droplet

Consider a fixed droplet in a stream of velocity U around it. The tangential shear stress at the surface of two-phase droplet is given as follows

$$\tau_{r\theta} = \mu_2 \left[r \frac{\partial}{\partial r}\left(\frac{u}{r}\right) + \frac{\partial \upsilon}{rd\theta} \right]_{r=b} \tag{5}$$

where μ_2 absolute viscosity of the immiscible liquid 2 (Fig. 2) , u is the radial component of fluid velocity, and υ is the tangential component of fluid velocity in the r, θ system of coordinates.

Substituting Eqs. (B4) and (B5) from Appendix B, into Eq. (5) gives the following after some algebra

$$\tau_{r\theta} = \frac{3\mu_2 U \sin\theta}{b(1-x)} \tag{6}$$

Utilizing the method of integrating the viscous dissipation function (Kendoush [9]), we get the following

$$E = \int_0^{\pi} \left[\tau_{r\theta}\upsilon\right]_{r=b} 2\pi b^2 \sin\theta d\theta \tag{7}$$

Substituting Eq. (6) and Eq. (B5) (Appendix B) into Eq. (7) gives the following

$$E = 8\pi b\mu_2 U^2 \frac{(x+\frac{1}{2})}{(1-x)^2} \tag{8}$$

The drag force is given as follows

$$F = \frac{E}{U} = 8\pi b\mu_2 U \frac{(x+\frac{1}{2})}{(1-x)^2} \tag{9}$$

The drag coefficient is defined by the following

$$C_D = \frac{F}{\frac{1}{2}\rho_{f2}U^2(\pi b^2)} \tag{10}$$

Substitution of Eq. (9) into Eq. (10) yields the following

$$C_D = \frac{32(x+\frac{1}{2})}{\mathrm{Re}(1-x)^2} \tag{11}$$

where $\mathrm{Re} = \rho_{f2}U(2b)/\mu_2$ is the Reynolds number

As $x \to 0$, the above equation reduces to that obtained by Moore [11]. This is also a new equation that has not been reported before, one of the merits of it, is the presence of the parameter x into it. This makes it useful for providing a fairly accurate balance between buoyancy and drag in the coming equation of motion.

2.3 The Equation of Motion

The droplet gets accelerated due to the continuous evaporation with the increase in size as shown in Fig.1. The unsteady motion of droplet is subjected to the following forces
(i) Buoyancy due to the density difference between the droplet and the continuous phase.
(ii) Buoyancy due to the vapor formation within the droplet
(iii) Drag on the surface of droplet
(iv) The impulse due to the virtual mass.
Accordingly, the equation of motion becomes the following

$$\frac{d}{dt}\left(\left[\frac{4}{3}\pi b^3\rho_{f1} + \frac{4}{3}\pi a^3\rho_{g1} + M\right]U\right) = \frac{4}{3}\pi b^3 g(\rho_{f2} - \rho_{f1}) + \frac{4}{3}\pi a^3 g(\rho_{f1} - \rho_{g1}) - F \tag{12}$$

Substituting for M and F from Eqs. (3) and (9) respectively into Eq.(12), we get the following

$$\frac{4}{3}\pi b^3 \rho_{f1}\frac{dU}{dt} + 4\pi\rho_{f1}Ub^2\frac{db}{dt} + \frac{4}{3}\pi a^3\rho_{g1}\frac{dU}{dt} + 4\pi\rho_{g1}Ua^2\frac{da}{dt} + \frac{2}{3}\pi\rho_{f2}\frac{a^3(1+2x)}{(1-x)}\frac{dU}{dt} +$$

$$2\pi\rho_{f2}a^2\frac{(1+2x)U}{(1-x)}\frac{db}{dt} + 2\pi\rho_{f2}\frac{a^3U}{(1-x)^2}\left(\frac{dx}{dt}\right) = \frac{4}{3}\pi b^3 g(\rho_{f2}-\rho_{f1}) + \frac{4}{3}\pi a^3 g(\rho_{f1}-\rho_{g1}) \qquad (13)$$

$$-8\pi b\mu_2 U\frac{(x+\frac{1}{2})}{(1-x)^2}$$

From Eq. (3), we get the following

$$\frac{dx}{dt} = 3b^{-3}a^2\frac{da}{dt} - 3b^{-4}a^3\frac{db}{dt} \qquad (14)$$

Assuming that $\frac{da}{dt} = \frac{db}{dt}$, this means that the growth in the size of the inner bubble will increase the size of the drop by the same magnitude. This assumption could be proved in a separate study. Consideration should be given to the displacement of the fluid inside the drop. The vapor pressure force aids this force. In opposition to these forces, there are the surface tension force of the drop and the local hydrostatic pressure force of the immiscible liquid. The above assumption, Eq. (14) and Eq. (2) gives the following

$$\frac{dx}{dt} = \frac{3x}{b}\left(\frac{b}{a}-1\right)\frac{da}{dt} \qquad (15)$$

Equation (13) will be solved for two different cases; the first is for low Jakob numbers , $Ja = \rho_{f2}cp_2\Delta T/\rho_{f1}\lambda$ that is, Ja < 16. Riznic et al. [12] recommended the following equation

$$a = \pi Ja\left(\frac{\alpha t}{3}\right)^{\frac{1}{2}} \qquad (16)$$

and

$$\frac{da}{dt} = \frac{\pi}{2}Ja\left(\frac{\alpha}{3t}\right)^{\frac{1}{2}} \qquad (17)$$

Substituting Eqs. (15-17) into Eq. (13) and simplifying, yields the following

$$\frac{dU}{dt}\left(\frac{2x^{-1/3}\rho_{f1}}{3} + \frac{2\rho_{g1}}{3x^{-2/3}} + \frac{\rho_{f2}x^{2/3}(1+2x)}{3(1-x)}\right)$$

$$+\frac{U}{t}\left(\rho_{f1} + \rho_{g1}x^{2/3} + \frac{\rho_{f1}x^{2/3}(1+2x)}{2(1-x)} + + \frac{3\rho_{f2}x^2(x^{-1/3}-1)}{(1-x)^2} + \frac{\rho_{f1}x^{2/3}(1+2x)}{2(1-x)}\right.$$

$$\left.+\frac{3\rho_{f1}x^2(x^{-1/3}-1)}{(1-x)^2}\right) = \frac{2g}{3x^{1/3}}(\rho_{f2}-\rho_{f1}) + \frac{2g(\rho_{f1}-\rho_{g1})}{3x^{-2/3}} - \frac{M_2 U\left(x+\frac{1}{2}\right)x^{1/3}}{\alpha Ja(1-x)t}$$

(18)

This equation will be solved for any fixed value of x, namely, 0.3, 0.5 and 0.7. For x=0.5 and utilizing the experimental data reported by Seleki and Gardon [2] for the evaporation of pentane drops in water. The following physical properties of pentane in water were used in Eq. (18) $\rho_{f1} = 3$ kg/m³, $\rho_{f2} = 997.4$ kg/m³, $\rho_{g1} = 3$kg/m³, $\mu_2 = 3.5 \times 10^{-4}$ kg/ms , $\alpha_2 = 0.0000001$ m²/s (α is the thermal diffusivity, and Ja=6.6. Accordingly, equation (18) becomes as follows

$$\frac{dU}{dt} + 4.2787\frac{U}{t} = 6.9947$$

(19)

This is a first order linear differential equation that can be solved by the integrating factor (I.F.) method as follows

$$I.F. = \exp\int 4.2787\frac{dt}{t} = t^{4.2787}$$

(20)

The solution of Eq.(19) becomes the following

$$Ut^{4.2787} = 1.325t^{5.2787} + C$$

(21)

where C is the constant of integration. The initial conditions are the following

$$\text{at } t = t_o \rightarrow U = U_o$$

(22)

Substituting Eq. (22) into Eq. (21) and evaluating C, yields the following

$$U = 1.325t + \left(\frac{t_o}{t}\right)^{4.2787}[U_o - 1.325t_o]$$

(23)

The travel distance of the droplet is obtained from the following

$$S = S_o + \int_{t_0}^{t} Udt$$

(24)

where S_o is the position of the droplet at the instant of separation from the nozzle. Substituting Eq. (23) into Eq. (24) and integrating, yields

$$S = S_o + 0.6625t^2 - \frac{t_o^{4.2787}}{t^{3.2787}}\frac{U_o}{3.2787} + \frac{1.325t_o^{5.2787}}{3.2787t^{3.2787}} - 1.325t_o^2 + \frac{t_o U_o}{3.2787}$$

(25)

The value of U_o was taken as 0.2m/s as it was given by various investigators, e.g. Ref. [1]. For this particular case t_o= 0.25 and S_o= 0.02 m. These values were obtained from Fig.3 of Selecki and Gradon [2].

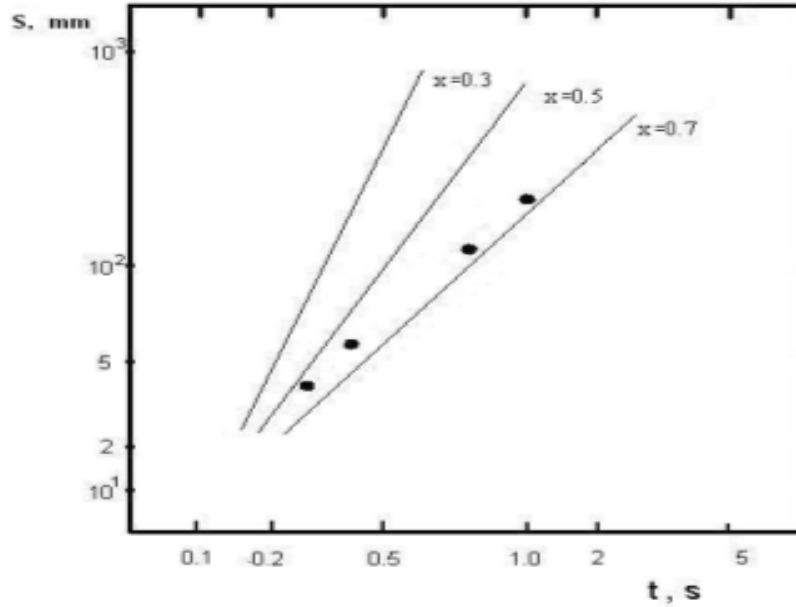Equation (25) was compared with the experimental data of Selecki and Gradon [2] in Fig.4.

Fig. 4 Comparison with Seleki and Gradon [2] , Ja= 6.58, △T=1.7 their number 1 in Fig. 3, ————— Eq. (25).

The calculation was repeated for high Jakob numbers, that is, Ja >16 with the following equation that was proposed by Riznic et al. [12]. This is the second case of solving Eq. (13).

$$a = \pi Ja(\frac{\alpha t}{3})^{\frac{1}{2}}$$ (26)

and

$$\frac{da}{dt} = \frac{\pi}{2} Ja\left(\frac{\alpha}{3t}\right)^{\frac{1}{2}}$$ (27)

Substituting Eqs. (26) and (27) into Eq. (13) with the same previous assumption of da / dt = db / dt, we get the following

$$\frac{dU}{dt}\left(\frac{\rho_{f1}x^{-1/3}}{3} + \frac{\rho_{g1}x^{2/3}}{3} + \frac{\rho_{f2}x^{2/3}(1+2x)}{6(1-x)}\right) + \frac{U}{t}\left(\frac{\rho_{f1}}{2} + \frac{\rho_{g1}x^{2/3}}{2} + \frac{\rho_{f2}x^{2/3}(1+2x)}{4(1-x)} + \frac{\rho_{f2}x(x^{-1/3}-1)}{(1-x)^2}\right)$$
$$= \frac{g}{3}x^{-1/3}(\rho_{f2} - \rho_{f1}) + \frac{g}{3}x^{2/3}(\rho_{f1} - \rho_{g1}) - \frac{18}{\pi}\frac{\mu_2}{\alpha Ja}\frac{(x+0.5)}{(1-x)^2}x^{1/3}$$

(28)

For x = 0.7, Ja = 50 and the same physical properties mentioned above, Eq. (28) becomes the following

$$\frac{dU}{dt} + 8.854\frac{U}{t} = 2.895 \qquad (29)$$

The I.F. = $t^{8.854}$ and the solution of Eq.(29) is the following

$$U = 0.2938t + \left(\frac{t_0}{t}\right)^{8.854}\left[U_0 - 0.2938t_0\right] \qquad (30)$$

The travel distance becomes for the same previous initial conditions

$$S = 0.02083 + 0.1469t^2 - \frac{7.395 \times 10^{-12}}{t^{7.854}} \qquad (31)$$

This equation was compared with the experimental data of Selecki and Gradon [2] in Fig. 5.
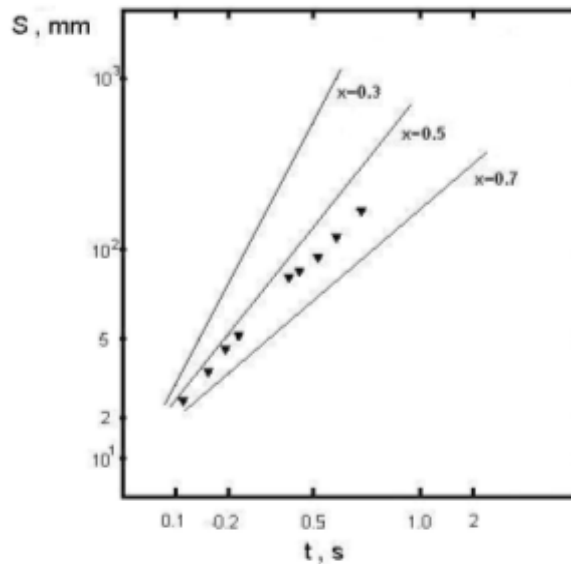

Fig. 5 Comparison with Seleki and Gradon [2], Ja = 50, $\triangle$T = 12.9
their number 1′ in Fig. 3, ——— Eq. (31).

3. Discussion

Figures 4 and 5 show an agreement between the present solution of the equation of motion and the available experimental date of the rise of pentane drop in water for both low and high Ja. Experimental recording of the travel distance of the evaporation drop starts from the nozzle tip, passing through the various stages of evaporation and shape

156-9

changing and finally into a complete bubble. The agreement between the present solution and the experimental data indicates the validity of the models developed for the virtual mass and the drag.

The present solution may be considered as a quasi steady state solution as it focuses on a particular state of evaporation, e.g. x=0.5 but registers the complete history of the droplet from the birth at the nozzle throat until it reaches the top of the column. The effect of the virtual mass is demonstrated in the present solution and the new model of the drag force seems to produce real and representative solution.

It should be noted that virtual mass coefficient of Eq.(4) is similar to that of Zuber [13] if one replaces x by the void fraction (α) in bubbly flow. Zuber's formula have been widely mentioned in the literature, e.g. by Wijngaarden [14] and Biesheuvel and Spoelstra [15]. Lamb's [8] derivation of the concentric spheres proved to have dual use. It either represents a cell within a swarm of bubble or it represents a spherical bubble formed within a drop.

A solution of the equation of motion was tried without the inclusion of the virtual mass term (that is, M in Eq. (3) was nullified). The result was an unrealistic solution that gives negative trajectory with time. In calculating forces on objects in fluids under transient conditions, the history effects, has to be included into the equation of motion. This term is responsible for the diffusion of vorticity around the object, and is, sometimes, called the Basset force (Michaelides [16]). The present analyses did not include this force into it as it was considered to be weak in comparison to the other forces. The following authors; Murai at al. [17] and Ohl et al. [18] reached the same conclusion. It should be noted that the contribution of the author [19] was mainly on the thermal side of the evaporating side of the droplet.

4. Conclusion

Analytical solutions were obtained for the virtual mass coefficient, drag coefficient and the equation of motion of a drop undergoing evaporation while it rises in an immiscible liquid. The following factors were assumed at the droplet:

- transient state
- inviscid and irrotational flow
- incompressible flow
- equal rates of growth for both the bubble and the drop outside it
- the bubble was assumed concentric inside the drop

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$$x = 1 - \frac{m}{m_o}$$

APPENDIX A: The Vaporization Ratio

If the vaporization ratio is defined as where m is the non evaporated mass of liquid within the drop and m_o is the initial mass of the dispersed drop, then

$$x = 1 - \frac{(4/3)\pi\rho_{f1}(b^3 - a^3)}{(4/3)\pi\rho_{f1}b^3}$$

or $x = (a/b)^3$

APPENDIX B : The Velocity Field

The velocity potential of the flow between two concentric spheres, is given by Lamb [8, page 124] as follows

$$\emptyset = \left(Ar + \frac{B}{r^2}\right)U\cos\theta \tag{B1}$$

If a , b are inner and outer sphere radii respectively, then

$$A = \frac{a^3}{b^3 - a^3} \quad \text{and} \quad B = \frac{1}{2}\frac{a^3 b^3}{b^3 - a^3}$$

The velocity components of the flow are obtained as follows

$$u = -\frac{\partial\phi}{\partial r} = \frac{U}{1-x}[x - (\frac{a}{r})^3]\cos\theta \dots\dots\dots\dots\dots\dots\dots\dots\dots\dots\dots\dots\dots\dots\dots\dots (B2)$$

and

$$\upsilon = -\frac{\partial\phi}{r\partial\phi} = \frac{U}{1-x}[x + \frac{1}{2}(\frac{a}{r})^3]\sin\theta \dots\dots\dots\dots\dots\dots\dots\dots\dots\dots\dots\dots\dots\dots (B3)$$

The vector $\frac{xU\cos\theta}{1-x}$ in Eq. (B2) and $\frac{xU\sin\theta}{1-x}$ in Eq. (B3) represent the main stream flow around the droplet b. If we want to set the droplet in motion in a stagnant fluid, we simply, remove this vector, this technique is essential in the derivation of drag forces, so we get the following

$$u = -(\frac{a}{r})^3 \frac{\cos\theta}{1-x}$$ ....(B4)

and

$$\upsilon = \frac{1}{2}(\frac{a}{r})^3 \frac{\sin\theta}{1-x}$$ ....(B5)