

Effect of Nanoparticles Size and Concentration on Thermal and Rheological Properties of AL₂O₃-Water Nanofluids

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Abstract - An experimental study was conducted to investigate the thermal and rheological properties of various suspensions of AL₂O₃ in deionized water. Tests were carried out using nanoparticles with average diameters of 5 and 50 nm for suspensions concentration ranging from 0 to 40% by mass. Tests reveal that alumina nanofluids thermal conductivity increases with the increase in operating temperature and in suspensions concentration, but decreases with the increase in nanoparticles diameter. Also, fluids with 5 nm particles exhibit non-Newtonian characteristics of shear thinning fluids. This behaviour intensifies as the suspensions concentration increases. However, fluids with 50 nm particles behave as shear thickening fluids. This behaviour does not seem to be altered by the increase in suspensions concentration. Tests also reveal that alumina nanofluids viscosity increases with the increase in the suspensions concentration. For fluids with 5 nm particles, viscosity is shown to increase with the increase in the operating temperature, but for fluids with 50 nm particles it is shown to decrease with the increase in temperature.

Keywords: nanofluid, nanoparticle, thermal conductivity, viscosity, non-Newtonian

1. Introduction

Thermal conductivity of AL₂O₃-water nanofluids have been experimentally examined in the past few years. However, there is a wide variation in the reported values among different authors. Very few researchers have examined the effect of using different particle sizes. Lee et al. [1] conducted studies on the thermal conductivity of dilute AL₂O₃-water nanofluids in a concentration range of 0.01 to 0.3% by volume using 30 nm AL₂O₃ particles. Their results showed an enhancement of 1.4% at 0.3% volume concentration. Chandrasekar et al. [2] performed tests for a larger concentration range of 0.3 to 3% by volume using 43 nm particles. The enhancement in thermal conductivity was about 10% for the concentration of 3% by volume. Mintsa et al. [3] investigated the effect of two different alumina particle sizes (36 and 47 nm) on the nanofluid thermal conductivity for concentrations ranging from 0 to 18% by volume. Their study showed the nanofluid thermal conductivity to increase with the decrease in nanoparticles size. At 18% volume concentration, the enhancement in the thermal conductivity of the nanofluid was about 30% for 36 nm particles, and 25% for 47 nm particles. A study performed by Das et al. [4] using 38.4 nm particles showed 9% enhancement in thermal conductivity at 4% volume concentration, while experiments performed by Ghanbarpour et al. [5] showed a much higher thermal conductivity enhancement. Their thermal conductivity enhancement was 16% at 4% volume concentration, and 88% at 12% volume concentration. Ghanbarpour et al. used larger alumina nanoparticles (75 nm). The study conducted by Duan [6] on nanofluid concentrations ranging from 0 to 5% by volume showed comparable results to Ghanbarpour et al. for that range. However, the nanoparticles he investigated were much smaller (25 nm). Eastman et al. [7] performed their tests in the same concentration range as Duan but with slightly larger particles (33 nm). The thermal conductivity enhancement was higher (24% at 4% volume concentration). On the other hand, Yiamsawasd et al. [8] reported a much lower enhancement of only 11% at 4% volume concentration for their 120 nm alumina particles. All of the above researchers have conducted their studies at room temperature with the exception of Mintsa et al. and Yiamsawasd et al. who have performed their tests at slightly elevated temperatures of 30 to 40 °C. There is contradiction among various researchers. For example, Lee et al. [1], Mintsa et al. [3], Das et al. [4] and Eastman et al. [7] have used comparable alumina nanoparticles ranging from 30 to 38 nm but have reported a wide variable in thermal conductivity where Mintsa et al. data were at the low end of values, and Eastman et al. data were at the high end. Also, inconsistencies are shown in the comparison of the data between Chandrasekar et al. [2] and Mintsa et al. [3] for their comparable nanoparticle size range of 43 to 47 nm. In addition, very

limited studies have investigated the effect of nanoparticle size on nanofluid thermal conductivity enhancement. The current study aims at resolving some of these issues by analyzing the thermal conductivity of alumina-in-water nanofluids, and the effect nanoparticles size have on the nanofluids thermal conductivity enhancement.

With regard to alumina-in-water viscosity, open literature review shows the research conducted on this nanofluid is still scarce. Some of the researchers who investigated alumina-in-water nanofluid viscosity include Timofeeva et al. [9], Murshed et al. [10], Nguyen et al. [11], and Yiamsawasd et al. [8]. These researchers have tested nanoparticles ranging in size from 11 to 75 nm. The majority of these researchers have investigated larger nanoparticles with the exception of Timofeeva et al. who were the only ones to examine the effect of nanoparticles as fine as 11 nm. Murshed et al. and Chandrasekar et al. have tested concentrations up to 5% by volume, and their results showed a viscosity increase between 80 to 140%, while the other researchers have increased their concentrations to 10% by volume and their viscosity has increased between 114 and 180%. The aim of this study is to expand on these findings.

2. Experimental Setup

The thermal conductivity of various suspensions of Al_2O_3 in deionized water was measured using a KD2 Pro thermal properties analyzer by Decagon Devices. The analyzer consists of a microcontroller with several needle sensors that can be used. KS-1 sensor needle was selected to determine the thermal conductivity of the nanofluids. The needle contains both a heating element and a thermistor. The needle, 1.3 mm in diameter and 6 cm long, was inserted vertically (to minimize natural convection) inside a test tube containing the nanofluid sample (Fig. 1). Heat was applied to the single needle for a short duration of time, and the temperature was monitored in the needle for an additional time after heating was turned off. The total time duration for each test was about 1 minute. The fluid sample was heated by a temperature-controlled water bath that was insulated from the surroundings. Tests were carried out after the desired steady state temperature of the fluid was reached. KD2-Pro thermal conductivity measurements are sensitive to temperature changes, and for this reason all measurements were done in a water bath. To eliminate forced vibration in the fluids, tests were carried out in the quiet evenings on a specially built vibration isolation table and away from environmental disturbances that are caused by systems such as HVAC, fans, electronic devices, and daily people activity. Repeated test measurements were performed on each nanofluid sample. Averaged values and uncertainty in the experimental determination of thermal conductivity were obtained.

Rheology tests were conducted on suspensions of Al_2O_3 in deionized water using a specially built UL adapter attached to LVDV-II+Pro Brookfield digital viscometer (Fig. 2). The UL adapter measures viscosities as low as 1 centipoise. Newtonian and non-Newtonian fluids can be tested. The UL adapter consists of a precision cylindrical spindle rotating inside an accurately machined tube that contains the 16 ml fluid test sample. A water jacket for accurate temperature control surrounds the tube.

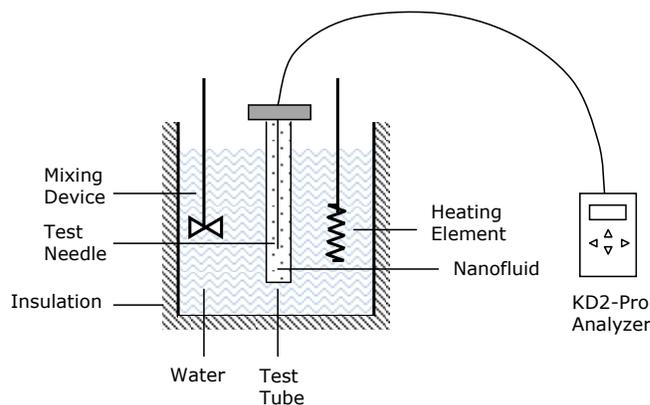


Fig. 1: Experimental setup for thermal conductivity analysis.



Fig. 2: LVDV-II+Pro viscometer (UL adapter).

3. Results and Discussion

3.1. Thermal Conductivity Measurements

Nanofluid test samples using 5 and 50 nm alumina particles of various concentrations were prepared and tested in a laboratory experimental setup for the determination of thermal conductivity. Figures 3 and 4 show the average thermal conductivity of repeated test measurements on 5 and 50 nm Al_2O_3 suspensions in deionized water, respectively. Tests were carried out at two different fluid temperatures (21.8-23 °C, and 46-46.5 °C), and for nanoparticles concentrations ranging from 0 to 20% by mass for the 5 nm suspensions, and from 0 to 40% by mass for the 50 nm suspensions. Figures 3 and 4 show the error bars associated with repeated tests. Tests reveal that the thermal conductivity of the nanofluid increases with the increase in fluid temperature, and also increases with the increase in Al_2O_3 mass concentration. A comparison in thermal conductivity values between Figs. 3 and 4 shows that a decrease in alumina nanoparticle size results in an increase in the thermal conductivity of the nanofluid. For the same mass concentration, as the particle size decreases, the number of particles in the base fluid increases causing an increase in the surface area between the solid and the liquid phase, thus resulting in an increase in the effective thermal conductivity. Results show thermal conductivity increases by about 33% for the case of 50 nm particles and 46 °C water bath temperature as the mass concentration increases from 0 to 20%. For the case of 5 nm particles and 46.5 °C water bath temperature, the increase in mass concentration from 0 to 20% results in an increase of about 38% in thermal conductivity. The decrease in alumina particle size from 50 to 5 nm results in an average increase of about 5% in thermal conductivity for the mass concentration range of 0 to 20%. The uncertainty in the determination of thermal conductivity is shown to increase with the increase in the suspensions concentration.

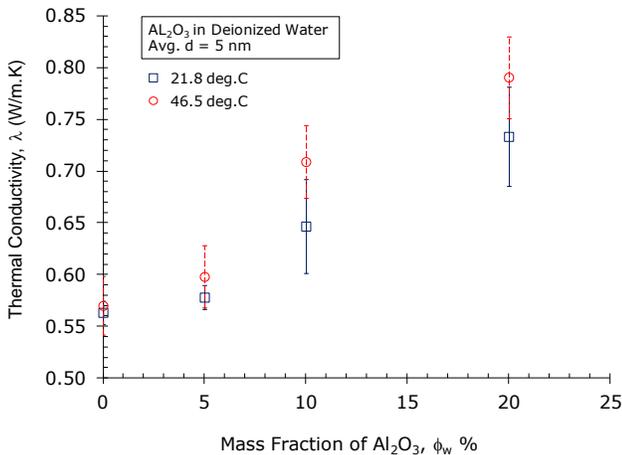


Fig. 3: Nanofluid thermal conductivity versus Al_2O_3 concentration by mass (5 nm particles).

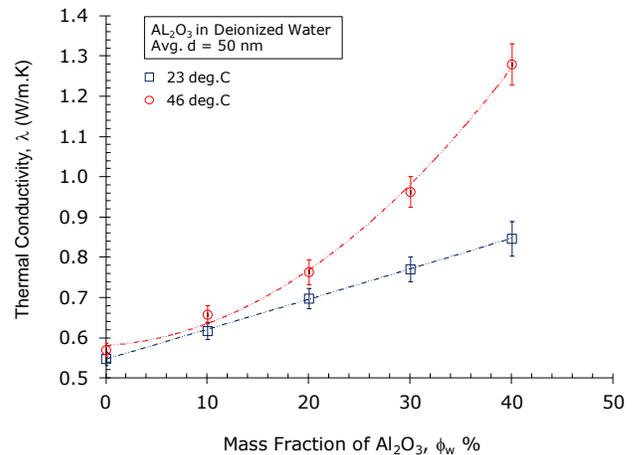


Fig. 4: Nanofluid thermal conductivity versus Al_2O_3 concentration by mass (50 nm particles).

Thermal conductivity of the nanofluids is estimated from the temperature history obtained by the thermal property analyzer using the relationship proposed by Carslaw and Jaeger [12]:

$$\lambda = \frac{q}{4\pi L} \frac{d \ln t}{d\Delta T} \quad (1)$$

Where λ is the fluid thermal conductivity of the nanofluid, q is the heating energy in the needle sensor, L is the length of the hot wire, t is time, and T is temperature.

3.2. Specific Heat Measurements

Calorimetric tests were conducted on the test samples to determine their specific heat (quenching of steel in water-based nanofluids with alumina). The following equation was used to estimate the specific heat of a nanofluid sample, c_{nf} :

$$c_{nf} = \frac{m_s c_s}{m_{nf}} \frac{T_{i,s} - T_{nf,f}}{T_{nf,f} - T_{nf,i}} \quad (2)$$

Where $T_{nf,i}$ is the initial temperature of the nanofluid sample, $T_{nf,f}$ is the final temperature of the nanofluid sample, $T_{i,s}$ is the initial temperature of the stainless steel sphere used in the calorimeter, c_s is the specific heat of the sphere, m_s is the mass of the spheres, and m_{nf} is the mass of the nanofluid sample. Figure 5 shows the specific heat of the nanofluid samples for the case of 5 and 50 nm particles as function of the particles mass concentration. The results show the specific heat to decrease with the increase in particles mass concentration. As the concentration increases from 0 to 20%, the decrease in the specific heat is by about 15% for the case of 50 nm suspensions and by about 20% for the case of 5 nm suspensions. It is also observed that as the nanoparticles size decreases from 50 to 5 nm, the specific heat decreases by an average of 5%.

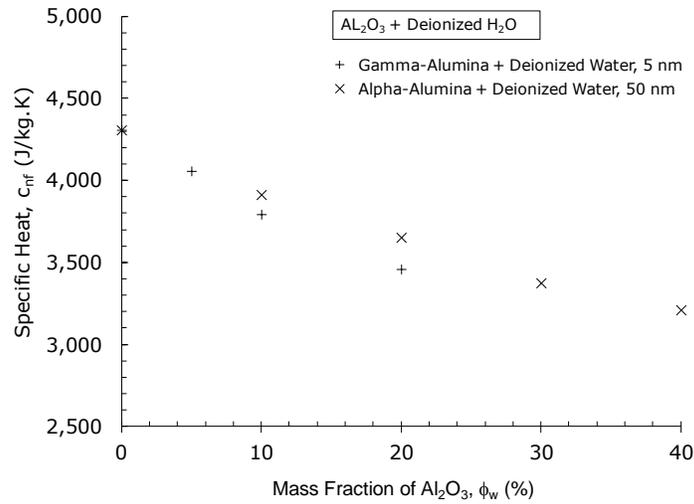


Fig. 5: Nanofluid specific heat versus AL₂O₃ concentration by mass.

3.3. Rheological Property Measurements

Rheological tests were conducted on the same samples originally used for thermal property evaluation. Rheological properties were conducted using UL adapter attached to LVDVII+Pro viscometer. Suspensions were mixed thoroughly using a high-speed mixing device for about 30 minutes before the viscosity tests were carried out. All tests were performed at room temperature ranging from 18 to 18.5 °C, and at an elevated temperature ranging from 45 to 47 °C using a water bath. Figure 6 shows the variation in the nanofluid viscosity as function of the shear rate, nanoparticles concentration, and operating temperature for the case of 5 nm particles. Figure 7 shows similar results for the case of 50 nm particles. Suspensions with 5 nm particles show a decrease in viscosity with the increase in shear rate. The viscosity is shown in Fig. 6 to decrease by a factor of 10 as shear rate increases by a factor of 100. This is a typical behaviour for a shear thinning fluid (pseudoplastic behaviour). For these nanofluids, viscosity increases with both particles concentration and operating temperature. However, suspensions with 50 nm particles show some increase in viscosity with the increase in shear rate; thus, a shear thickening fluid behaviour (dilatant fluid). The maximum increase in viscosity seen in Fig. 7 is by a factor of about 2 for a shear rate increase by a factor of 3. Figures 8 and 9 show the shear stress as function of shear rate, concentration and temperature for the 5 and 50 nm particles suspensions, respectively.

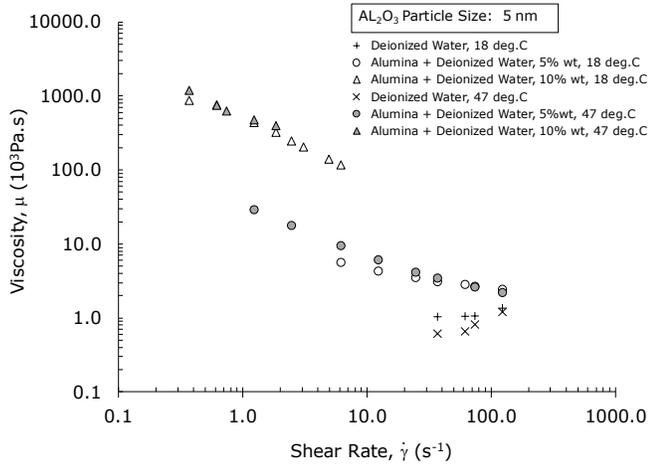


Fig. 6: Viscosity versus shear rate (5 nm particles).

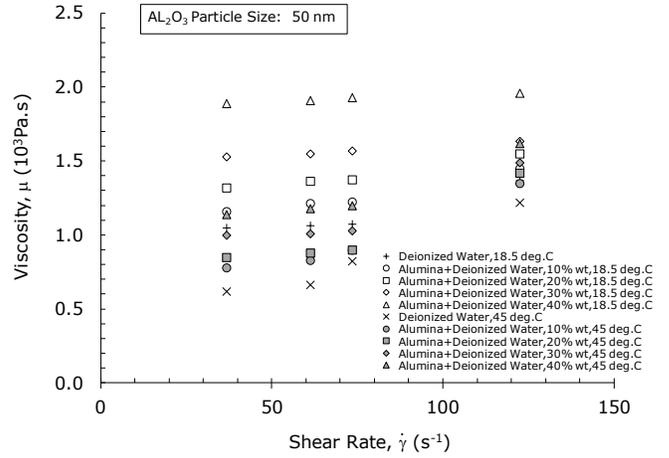


Fig. 7: Viscosity versus shear rate (50 nm particles).

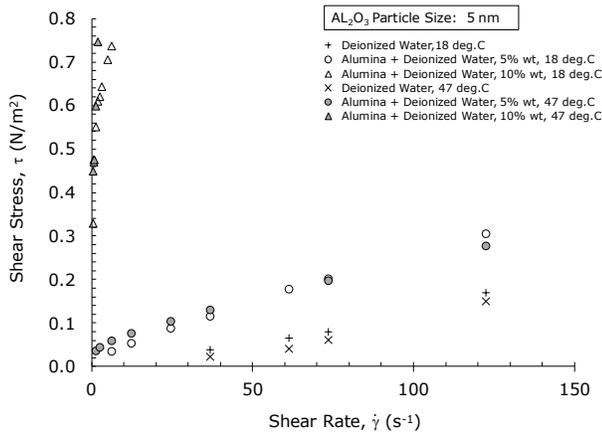


Fig. 8: Shear stress versus shear rate (5 nm particles).

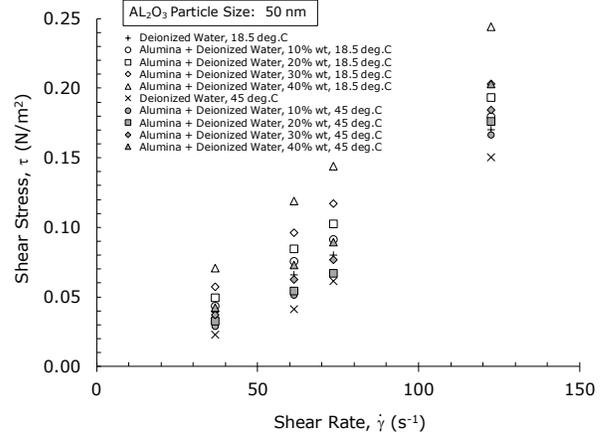


Fig. 9: Shear stress versus shear rate (50 nm particles).

For the case of 5 nm particles suspensions (Fig. 8), the fluids are shown to exhibit non-Newtonian flow behaviour. This relationship can be represented by the power law or Ostwald-de-Wale equation:

$$\tau = K\dot{\gamma}^n \quad (3)$$

Where K is a consistency coefficient and n is the power law index of the flow. n can be experimentally determined from the slope of the double logarithmic plot for the viscometer motor torque, T_m , versus spindle angular velocity, ω :

$$n = \frac{d \ln T_m}{d \ln \omega} \quad (4)$$

n is less than 1 for pseudoplastic fluids, greater than 1 for dilatants fluids, and equal to 1 for Newtonian fluids. For the case of 5 nm particles suspensions (Fig. 8), as the particles mass concentration increases from 5 to 10%, the fluids non-Newtonian characteristics intensify. For mass concentrations of 10%, the fluids behave as Bingham pseudoplastic where a finite yield stress is required before the fluids begin to flow. However, for the case of 50 nm particles suspensions (Fig. 9), the fluids exhibit slight non-Newtonian characteristics. The increase in concentration does not seem to alter this behaviour.

Table 1 shows the calculated power law index (for the test cases in Figs. 6 through 9) to vary from 0.25 to 0.72 for the 5 nm particles and from 1.03 to 1.45 for the 50 nm particles revealing shear thinning and shear thickening behaviours.

Table 1: Calculated power law index parameters for the nanofluids.

Nanoparticles Size (nm)	Mass Concentration (%)	Fluid Temperature (°C)	Power Law Index, n	Consistency, K ($\times 10^3$)	Least Square Fit, r^2
5	5	18.0	0.722	9.080	0.997
5	10	18.0	0.253	490.1	0.910
5	5	47.0	0.433	29.38	0.976
5	10	47.0	0.325	574.0	0.888
50	10	18.5	1.171	0.625	0.996
50	20	18.5	1.128	0.835	0.997
50	30	18.5	1.049	1.303	1.000
50	40	18.5	1.027	1.749	1.000
50	10	45.0	1.448	0.145	0.982
50	20	45.0	1.390	0.197	0.964
50	30	45.0	1.322	0.292	0.976
50	40	45.0	1.294	0.377	0.984

3.4. Comparison with other Studies

Figure 10 shows a comparison in the thermal conductivity of alumina-in-water nanofluids between the current study and other studies. The results of the current study compared well with those of Eastman et al. [7] and Ghanbarpour et al. [5]. The current study and Eastman et al. used the transient hot wire method for determining thermal conductivity, while Ghanbarpour et al. used the transient plane source method and a surfactant in the nanofluid. These studies showed much higher thermal conductivities than the other studies in the figure. For example, the study by Mintsä et al. [3] was also based on the transient hot wire method, but their thermal conductivity was much lower. In their tests, a mixer was embedded all the time at a very close proximity to the sensor and may have altered the data. However, results of others such as Duan [6], who also used the transient hot wire method and a surfactant, were not too far off.

Figure 11 shows a comparison in the viscosity of alumina-in-water nanofluids between various studies. For the case of 50 nm particles, the results of the current study compared well with those of Ghanbarpour et al. [5] and Nguyen et al. [11], but were not far off from the results of others as long as the particles size was between 40 and 75 nm. However, for the case of 5 nm particles, the results of the current study showed the nanofluid becoming extremely viscous with the increase in particles concentration. Research using very fine particles is scarce except those by Timofeeva et al. [9] for 11 nm particles. For these very fine particles, a similar trend in the viscosity behaviour is shown.

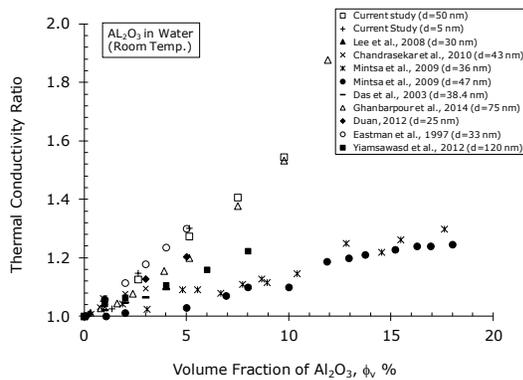


Fig. 10: Thermal conductivity comparison between various studies.

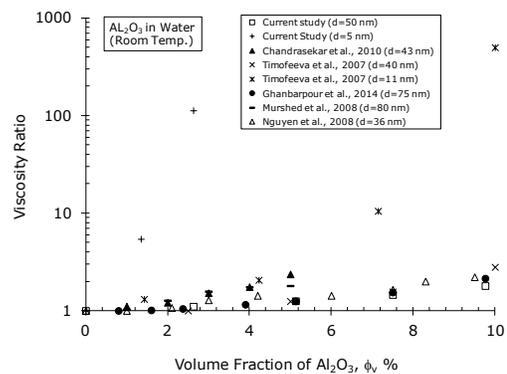


Fig. 11: Viscosity comparison between various studies.

4. Conclusion

An experimental study was conducted to investigate the thermal and rheological properties of alumina-in-water nanofluids. Tests were carried out on suspensions concentration ranging from 0 to 40% by mass and for particle sizes of 5 and 50 nm. Tests reveal that as the mass concentration increases from 0 to 20%, thermal conductivity increases by about 33% for the 50 nm particles and by about 38% for the 5 nm particles. The decrease in nanoparticle size results in about 5% improvement in bulk thermal conductivity. Specific heat is shown to decrease with the increase in nanoparticles concentration, and also to decrease with the decrease in nanoparticles size. Rheological tests on suspensions using 5 nm particles show a sharp decrease in viscosity with the increase in shear rate (pseudoplastic behaviour). The decrease in viscosity is by about a factor of 10 as shear rate increases by a factor of 100. However, suspensions using 50 nm particles show an increase in viscosity with the increase in shear rate (dilatant fluid). The maximum increase in viscosity is by a factor of less than 2 as shear rate increases by a factor of 3. The decrease in particle size from 50 nm to 5 nm causes an increase in viscosity by as much as 1000% at very low shear rates. Viscosity is also shown to increase with both particles concentration and operating temperature.

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